

# Specializing in Thermal Management via IR Sensing







# Industrial Division



#### EXERGENIR Sensors





# Increasing Production Speeds via Heat Balance Control With IR Sensing

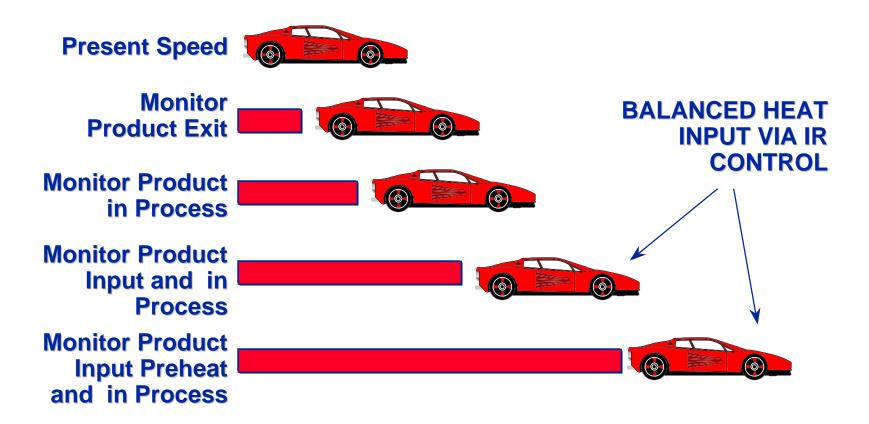
From Fundamentals to Frontiers







#### Speed Increase Stages







#### **Fundamentals**

- Infrared Physics and Math (Briefly)
- Emissivity High and Low
- Principles of the IRt/c in Non-Contact Temperature Measurement
- Heat Transfer Physics and Math (Briefly)





#### **Frontiers**

- Principles of the Heat Balance in Time and Space
- The Speed Boost Equation
- Balanced Heat Input via IR Control
- Applications
  - Laminating, Drying, Printing, Heat Sealing, Color Copying
- High Speed Event Detection

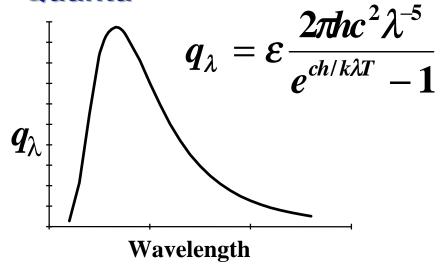




#### Max Planck ~ 1900



- Desparation Move to Explain Black Body Radiation
- Mathematical Equation for Thermal Radiation Using Quanta







#### Albert Einstein ~ 1905

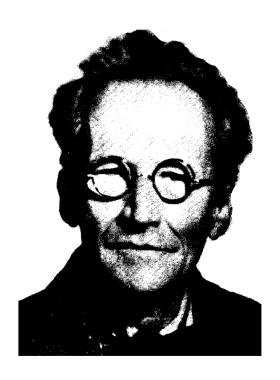


- Confirmed Planck's Quanta by Explanation of Photoelectric Effect
- But Never Really Liked the Eventual Result

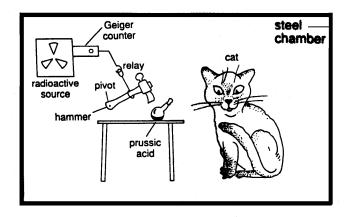


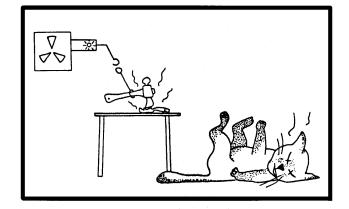


# Erwin Schrodinger ~ 1935



#### The Cat Paradox









#### Basic Infrared Equations

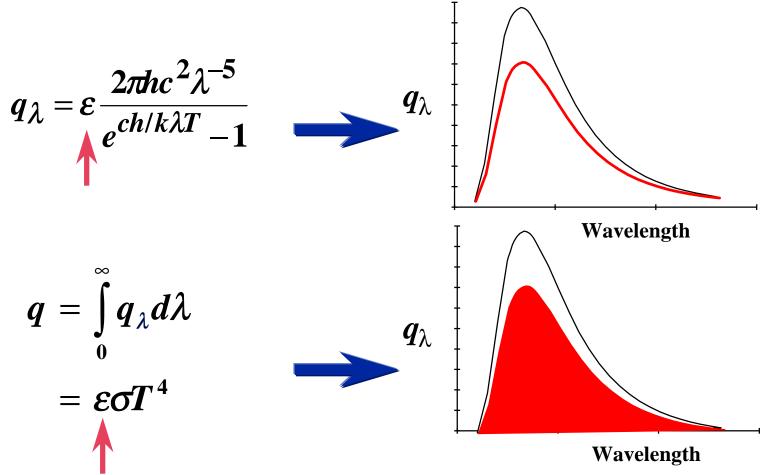
$$q_{\lambda} = \frac{2\pi hc^2 \lambda^{-5}}{e^{ch/k\lambda T} - 1}$$
  $\longrightarrow$   $q_{\lambda}$ 

$$q = \int_{0}^{\infty} q_{\lambda} d\lambda$$
  $\longrightarrow$   $q_{\lambda}$ 

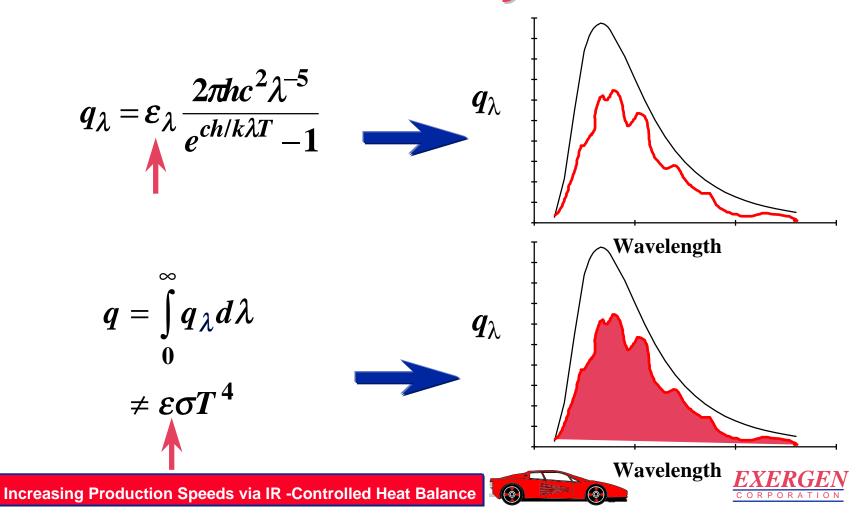
$$q_{\lambda} = \sigma T^4$$
Wavelength



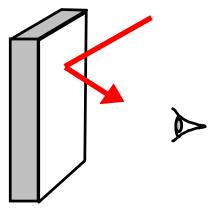
#### **Emissivity**



#### Wavelength Dependent Emissivity

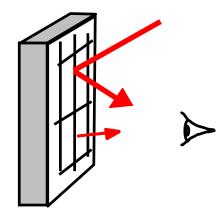


#### Low Emissivity Surfaces



#### **Perfect Mirror**

Emissivity = 0.0Reflectivity = 1.0



#### **Poor Emitter**

Emissivity = 0.1Reflectivity = 0.9

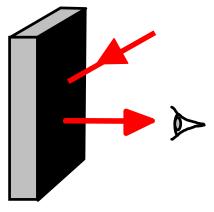
**Theoretical** 

### Real: Uncoated Metals





#### High Emissivity Surfaces

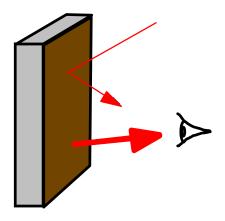


#### **Perfect Blackbody**

Emissivity = 1.0Reflectivity = 0.0

1.0

**Theoretical** 



#### **Good Emitter**

Emissivity = 0.9

Reflectivity = 0.1

1.0

Real: Non-Metals





# Measuring High Emissivity Surfaces

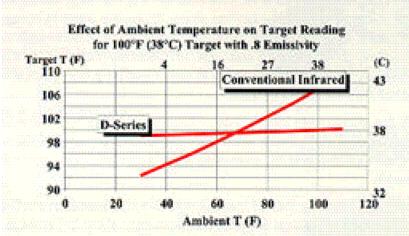
- Use Sensors Designed For High Emissivity
- Calibrate Sensors to Actual Material in Production Process for High Accuracy
- Use D-Series to Determine Accurate Temperature for Calibration





# D-Series: Measure True Temperature for Calibration





- Reflective cup provides true emissivity-free, and reflection-free temperature measurement
- Primary standard for calibration of IR sensor installations





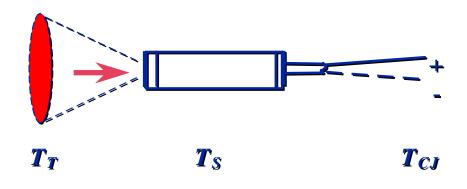
# Measuring Low Emissivity Surfaces

- Coat the Surface, Then Use High Emissivity
   If Not, Then
- Use Sensors Designed For Low Emissivity
- Calibrate Sensors to Actual Material in Production Process for High Accuracy
- Use D-Series to Determine Accurate Temperature for Calibration
- Use Cavities if Available on the Part





#### Principles of the IRt/c



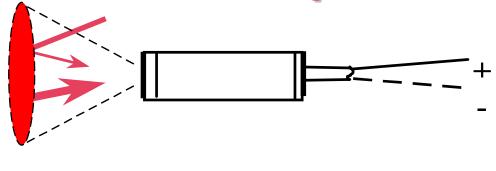
$$mV_{out} = c (T_T - T_S) + \alpha (T_S - T_{CJ})$$
  
=  $\alpha (T_T - T_{CJ})$  when  $c = \alpha$   
 $\alpha = Seebeck coefficient$ 

- No Power Required
- T/C Compatible
- 0.0001°C
   Resolution
- 0.01°C
   Repeatability
- Intrinsically Safe
- Simple, Rugged, Inexpensive





#### Principles of the IRt/c



$$T_T$$
  $T_S$   $T_{CJ}$ 

$$mV_{out} = c(\varepsilon T_T + (1-\varepsilon)T_S - T_S) + \alpha(T_S - T_{CJ})$$
  
=  $\alpha(T_T - T_{CJ})$  when  $(c \varepsilon) = \alpha$   
 $\alpha = Seebeck coefficient$ 

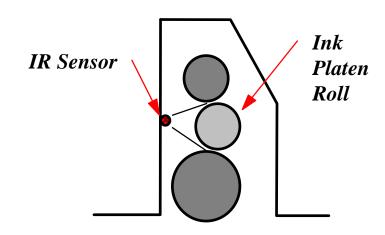
- Calibrated to Real World Surfaces to Reduce Errors Caused by Emissivity < 1</li>
- Optimum
   Temperature Range
   Selection for
   Highest Possible
   Accuracy in Real
   World Applications

Compensates for the Ambient Reflections on Real Surfaces





## Example of Improved Accuracy: Printing



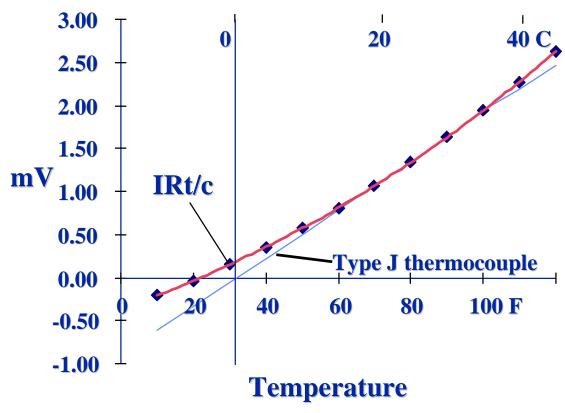
IR Temperature Control Accuracy:

Conventional IR	<i>3°F (1.7°C)</i>
IRt/c	$0.2^{\circ}F(0.1^{\circ}C)$





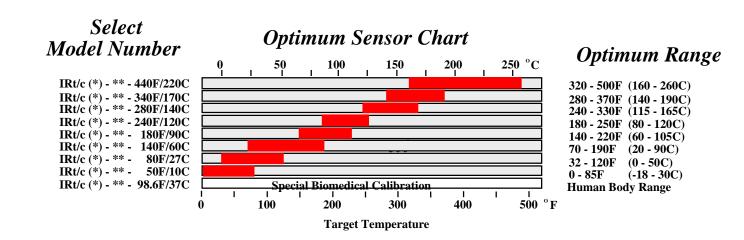
#### IRt/c Signal Output







#### Optimum Temperature Range Selection for Highest Possible Accuracy in Real World Applications







## Signal Output Polynomials For User Programming

#### Master Polynomial Table for IRt/c Signal Output

B C D E

 $(TT - CJT) = A*(mV)^6 + B*(mV)^5 + C*(mV)^4 + D*(mV)^3 + E*(mV)^2 + F*(mV) + G$ 

	71	D		D	L	•	Ü
IRt/c.xxx - J - 50F/10C	-6.14473E-0	9 2.08199E-06	-2.72953E-04	4 1.75317E-02	-5.84883E-0	1 1.53005E+01	0
IRt/c.xxx - J - 80F/27C	-2.83996E-0	8 7.41635E-06	-7.54046E-04	4 3.79224E-02	-1.00406E+0	0 2.06592E+0	10
IRt/c.xxx - J - 140F/60C	-4.31591E-0	8 1.06077E-05	-1.01002E-03	3 4.72155E-02	-1.14872E+0	0 2.20397E+0	10
IRt/c.xxx - J - 180F/90C	-7.03138E-0	8 1.59317E-05	-1.39844E-03	3 6.02655E-02	-1.35167E+0	0 2.39075E+0	10
IRt/c.xxx - J - 240F/120C	-1.05707E-0	7 2.23776E-05	-1.83521E-03	3 7.38926E-02	-1.54843E+0	0 2.55885E+0	10
IRt/c.xxx - J - 280F/140C	-1.89514E-0	7 3.63996E-05	-2.70839E-03	3 9.89395E-02	-1.88106E+0	0 2.82034E+0	10
IRt/c.xxx - J - 340F/170C	-2.99852E-0	7 5.33519E-05	-3.67751E-03	3 1.24452E-01	-2.19192E+0	0 3.04447E+0	10
IRt/c.xxx - J - 440F/220C	-5.20472E-0	7 8.44263E-05	-5.30444E-03	3 1.63572E-01	-2.62438E+0	0 3.31770E+0	10





G

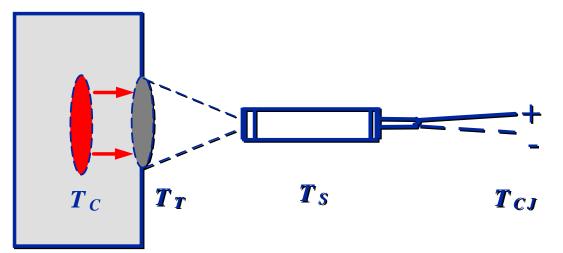
A

# Thermal Energy Balance in Space and Time: The Space Domain





# Principles of the IRt/c: With Heat Balance



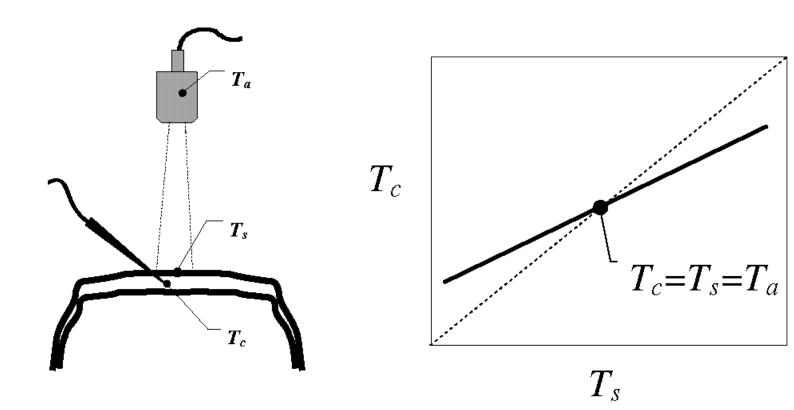
- Automatically
   Computes Heat
   Balance, Using
   Material Properties
   Alone
- Can be Configured for Unpowered or Powered Configurations

$$mV_{out} = c((T_C - T_S)(1/k) + T_S - T_S) + \alpha(T_S - T_{CJ})$$
  
=  $\alpha(T_C - T_{CJ})$  when  $c = (\alpha k)$   
 $\alpha = Seebeck coefficient$ 





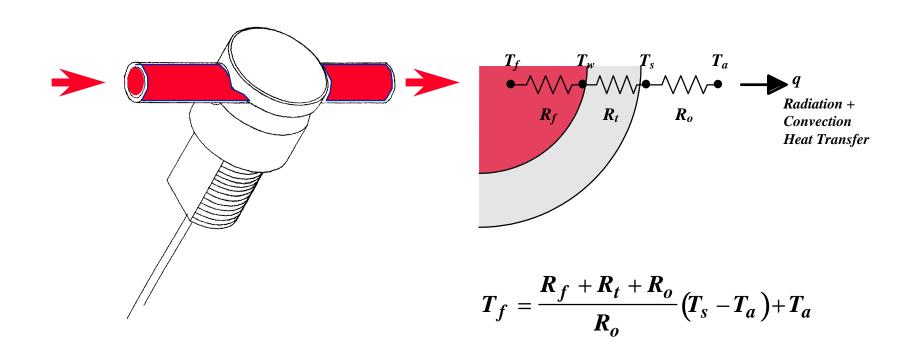
## Heat Balance Example: Internal Tire Temperatures







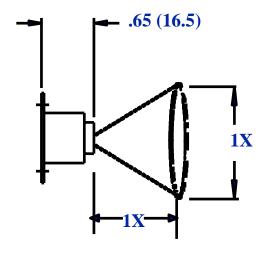
# Non-Invasive Fluid Temperature in Tubing via IRt/c Heat Balance

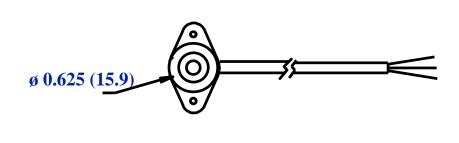






# Ultra-Miniature Infrared Thermocouple With Heat Balance









# Thermal Energy Balance in Space and Time: The <u>Time</u> Domain





## Jean Baptiste Joseph Fourier 1768-1830

Fourier's Equation of Heat Conduction

$$\left(\frac{q}{A}\right)_{x} = -k\frac{\partial T}{\partial x}$$

 Unsteady State Heat Conduction for Moving Materials

$$\frac{\partial^2 T}{\partial x^2} = \frac{1}{\kappa} \frac{\partial T}{\partial t}$$





### Pierre Simon Marquis de <u>LaPlace</u>

Laplace Transform Method of Solution

$$\overline{T}(x,s) = \int_{0}^{\infty} e^{-st} T(x,t) dt$$

 Converts Partial Differential Equation to Ordinary Differential Equation

$$\frac{d^2 \overline{T}}{dx^2} - \frac{s}{\kappa} \overline{T} = \frac{T_o}{\kappa}$$





## Francesco Pompei

 New Method of Solution Leads to a General Equation for Non-Contact Temperature Monitoring of <u>Internal</u> Temperatures of Moving Materials

$$T_{c} = \frac{h\sqrt{\tau\kappa}}{k} \sinh\left(\frac{a}{\sqrt{\tau\kappa}}\right) \left(T_{s} - T_{\infty}\right) + T_{s} + \left[\cosh\left(\frac{a}{\sqrt{\tau\kappa}}\right) - 1\right] \left(T_{s} - T_{0}\right)$$





#### Which simplifies to

$$T_c = K_1(T_s - T_{\infty}) + T_s + K_2(T_s - T_o)$$

where

$$K_1 = \frac{1}{a} \sqrt{\tau \kappa} \frac{ha}{k} \sinh \left( a \sqrt{\frac{1}{\tau \kappa}} \right)$$
,  $K_2 = \left( \cosh \left( a \sqrt{\frac{1}{\tau \kappa}} \right) - 1 \right)$ 

$$\frac{1}{a}\sqrt{\tau\kappa} = (Fo)^{1/2}$$
 , and  $\frac{ha}{k} = Bi$ 





#### Deriving The Speed Boost Equation

$$T_c = K_1(T_s - T_{\infty}) + T_s + K_2(T_s - T_o)$$

 Set the surface temperature equal to the center temperature, then the equation reduces to

$$T_c = T_s$$

$$\frac{(T_{\infty} - T_s)}{(T_s - T_o)} = \frac{K_2}{K_1}$$

 Since K<sub>2</sub>/K<sub>1</sub> is a function only of material properties and speed:





The ratio can be formed, which then becomes:

#### The Speed Boost Equation

$$rac{m{V_{new}}}{m{V_{old}}} = rac{\left(\overline{\Delta T}
ight)_{new}}{\left(\overline{\Delta T}
ight)_{old}}, \quad where \ \overline{\Delta T} = rac{m{T}_{\infty} - m{T}_{s}}{m{T}_{s} - m{T}_{o}}$$

- General Equation for Non-Contact IR Temperature Monitoring of <u>Internal</u> Temperatures of Moving Materials is Combined with Surface Temperature
- Leads to Uniform Material Temperature When Controlled via the <u>Speed Boost Equation</u>
- Which Forces the Control System to Apply Heat at an Optimally <u>Balanced</u> Rate

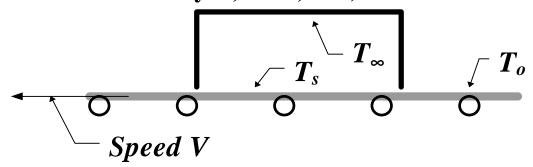




# Applying The Speed Boost Equation

$$rac{V_{new}}{V_{old}} = rac{\left(\overline{\Delta T}\right)_{new}}{\left(\overline{\Delta T}\right)_{old}}, \quad where \ \overline{\Delta T} = rac{T_{\infty} - T_{s}}{T_{s} - T_{o}}$$

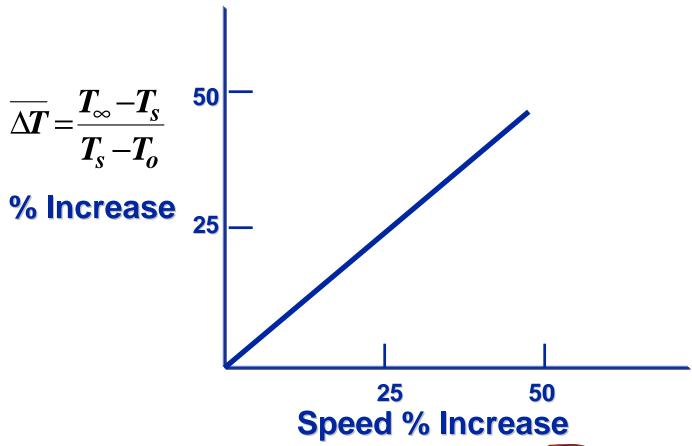
Thermal Input (oven, dryer, rolls, etc.)







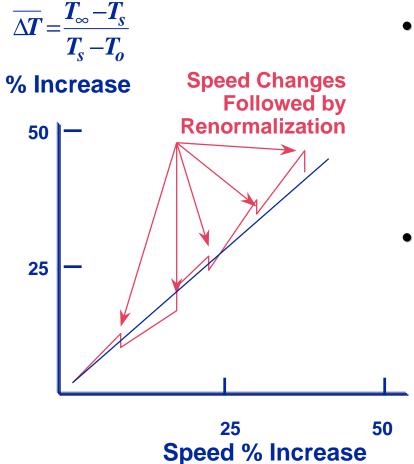
#### Speed Boost Equation is Generally Linear for Most Applications







# Implementing Speed Boost to Include Non-Linearities



- Apply step-wise speed increases in accordance with speed boost equation, and renormalize at new operating condition to account for property changes.
- For variable speed systems, program to follow the characteristic curve.





#### Example Speed Boost: Laminating

#### Existing Set-up:

$$T_{oo} = 105 C$$

$$T_{s} = 85 C$$

$$T_{o} = 25C$$

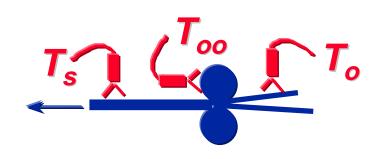
#### New Set-up:

$$T_{00} = 120 \text{ C}$$

$$T_{s} = 85 C$$

$$T_0 = 25C$$

 Potential Speed Increase\*:



$$\overline{\Delta T} = \frac{T_{\infty} - T_{S}}{T_{S} - T_{o}}$$

\*Assuming all other factors are permitting





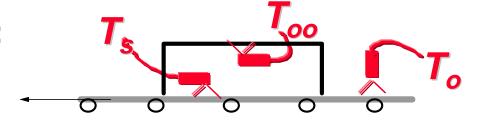
#### Example Speed Boost: Drying

#### Existing Set-up:

$$T_{oo} = 260 C$$

$$T_{s} = 85 C$$

$$T_{o} = 25 C$$



#### New Set-up:

$$T_{00} = 260 \text{ C}$$

$$T_{s} = 85 C$$

 $T_o = 40 C$  (with preheat)

#### Potential Speed Increase\*:

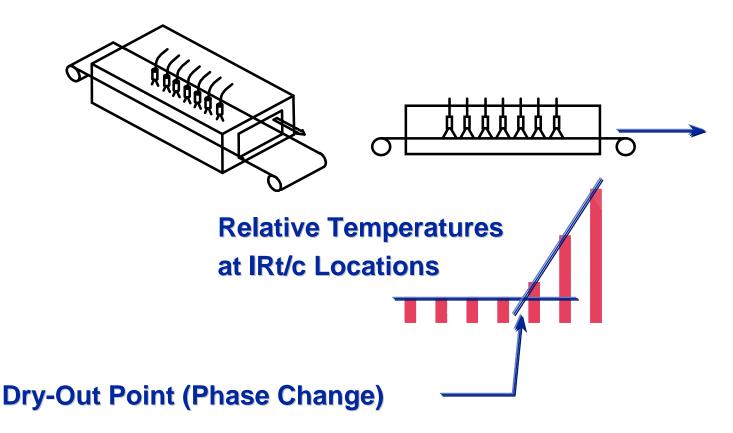
$$\overline{\Delta T} = \frac{T_{\infty} - T_{S}}{T_{S} - T_{o}}$$

\*Assuming all other factors are permitting





## Precision Drying Control for Maximum Production Speed







#### Example Speed Boost: Heat Sealing

Existing Set-up:

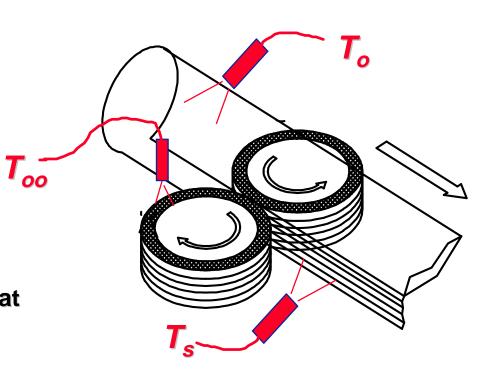
$$T_{oo} = 150 C$$
  
 $T_{s} = 120 C$ 

$$T_{o} = 25 C$$

New Set-up:

$$T_{oo}$$
 = 150 C  
 $T_{s}$  = 120 C  
 $T_{o}$  = 45 C (with preheat added)

 Potential Speed Increase:

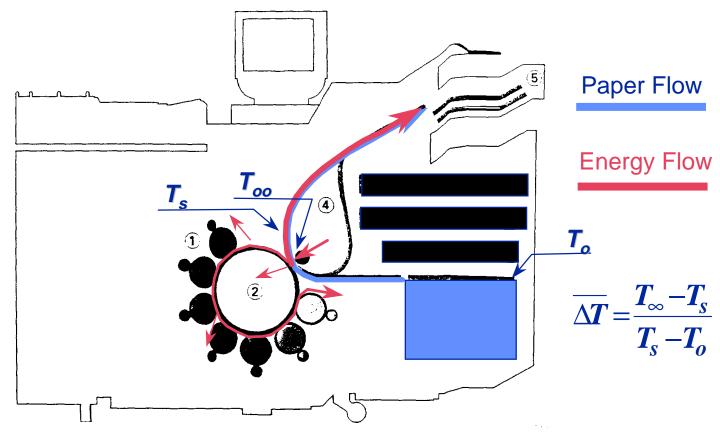


$$\overline{\Delta T} = \frac{T_{\infty} - T_{S}}{T_{S} - T_{O}}$$





# Example: High Speed Color Copy Process







### Speed Boost Equation

$$rac{V_{new}}{V_{old}} = rac{\left(\overline{\Delta T}\right)_{new}}{\left(\overline{\Delta T}\right)_{old}}, \quad where \ \overline{\Delta T} = rac{T_{\infty} - T_{s}}{T_{s} - T_{o}}$$

 Above Can Be a Simplified Control Algorithm

$$T_{\infty} = (\overline{\Delta T} + 1)(T_S) - (\overline{\Delta T})(T_O)$$
Heat Source Temperature

Product Surface setpoint

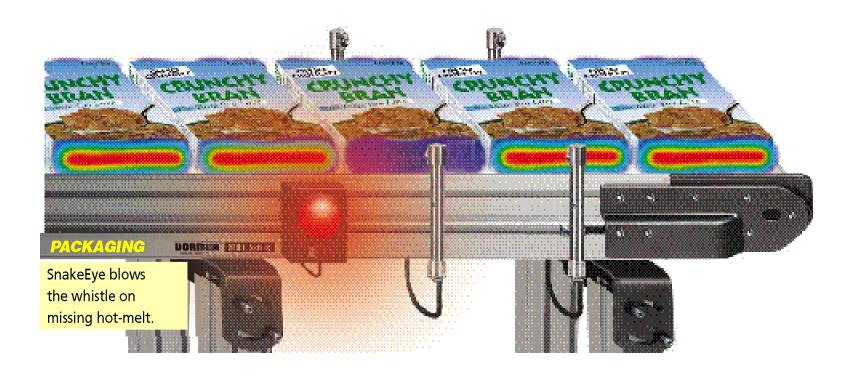
Product Input

 Keep Equation Balanced to Within a Few % to Avoid Non-Uniformity in Material Temperature





## **SnakeEye** Photocell-Like Non-Contact Thermal Inspection

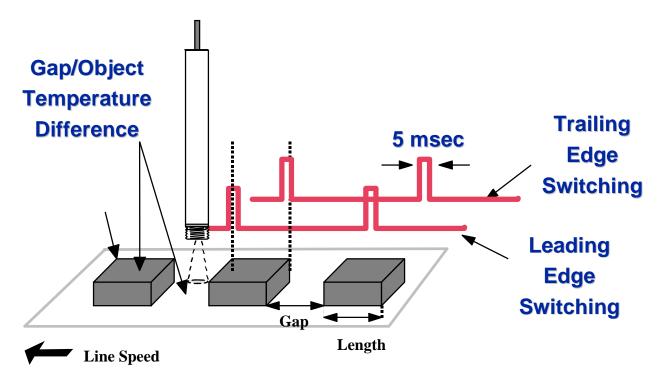






## **SnakeEye** Photocell-Like Non-Contact Thermal Switches

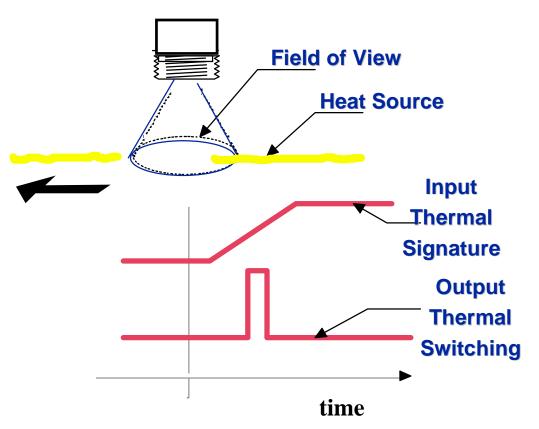
## Thermal Switching of Objects With Less Than 1°C Differential







### Principles of the SnakeEye



- The heat source enters the field-ofview of the SnakeEye and is detected by the sensing system.
- If the rate of change is of sufficient magnitude the SnakeEye causes the output to switch.





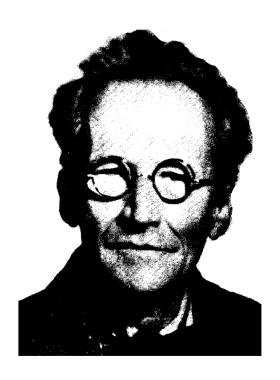
# Detecting Presence/Absence Hidden Foil Safety Seal

**Heat Signature of Heated Foil Through Cap Pharmaceutical Bottle Induction Heater** 

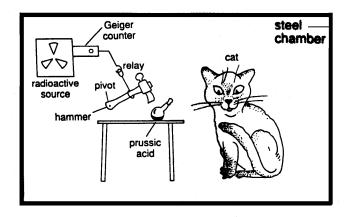


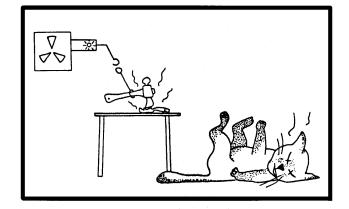


# Erwin Schrodinger ~ 1935



#### The Cat Paradox









# You Cannot Know For Sure That the Product is Right Unless You Look...

# With EXERGENIR Sensors





### The Exergen Creed

We are the best in the world at what we do,

And our products and services must be commensurate with our mission of supplying our customers with the best,

To help them be the best in the world at what they do.

F. Pompei
President and Founder

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